

(19) World Intellectual Property
Organization
International Bureau



(43) International Publication Date
17 February 2005 (17.02.2005)

PCT

(10) International Publication Number
WO 2005/015584 A2

(51) International Patent Classification⁷:

H01G

(21) International Application Number:

PCT/US2004/025582

(22) International Filing Date: 6 August 2004 (06.08.2004)

(25) Filing Language:

English

(26) Publication Language:

English

(30) Priority Data:

60/492,938

6 August 2003 (06.08.2003)

US

(71) Applicant (for all designated States except US):
BIOSOURCE, INC [US/US]; 1200 Millbury Street,
Suite 7F, Worcester, MA 01607 (US).

(72) Inventors; and

(75) Inventors/Applicants (for US only): **ANDELMAN,**
Marc, D. [US/US]; 1200 Millbury Street, Suite 7F,
Worcester, MA 01607 (US). **KURAN, Shihab** [JO/US];
507 Cardinal Lane, Green Brook, NJ 08812 (US).
ZULKIEWICZ, Jon [US/US]; 34 Mt. Dumplin Road,
Palmer, MA 01069 (US).

(74) Agent: **MEYER-LEON, Leslie**; IP Legal Strategies
Group P.C., 1480 Falmouth Road, P.O. Box 1210, Center-
ville, MA 02632-1210 (US).

(81) Designated States (unless otherwise indicated, for every
kind of national protection available): AE, AG, AL, AM,
AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN,
CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, EG, ES, FI,
GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE,
KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD,
MG, MK, MN, MW, MX, MZ, NA, NI, NO, NZ, OM, PG,
PH, PL, PT, RO, RU, SC, SD, SE, SG, SK, SL, SY, TJ, TM,
TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, YU, ZA, ZM,
ZW.

(84) Designated States (unless otherwise indicated, for every
kind of regional protection available): ARIPO (BW, GH,
GM, KE, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM,
ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM),
European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI,
FR, GB, GR, HU, IE, IT, LU, MC, NL, PL, PT, RO, SE, SI,
SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ,
GW, ML, MR, NE, SN, TD, TG).

Published:

— without international search report and to be republished
upon receipt of that report

For two-letter codes and other abbreviations, refer to the "Guid-
ance Notes on Codes and Abbreviations" appearing at the begin-
ning of each regular issue of the PCT Gazette.

(54) Title: POWER EFFICIENT FLOW THROUGH CAPACITOR SYSTEM

(57) Abstract: The invention features a flow-through capacitor system that achieves enhanced power efficiency by sequential control and actuation of at least two or more flow-through capacitor cells within the flow-through capacitor system. Alternatively or in addition, power efficiency is enhanced by integrating the purification stages of the system, for example, by placing more than one cell within a single cell casing. Preferably, integrated stage flow-through capacitors are controlled sequentially.

WO 2005/015584 A2

POWER EFFICIENT FLOW THROUGH CAPACITOR SYSTEM

Reference To Prior Application

5 This application is based on and claims priority from U.S. provisional patent application serial no. 60/492,938, filed August 6, 2003, which is hereby incorporated by reference.

Field of The Invention

 The field of the invention is systems for capacitive deionization of fluids by
10 the use of flow through capacitors.

Background of the invention

 It is generally recognized that, in order to purify concentrated water, flow-through capacitor purification systems need to be staged. It is an objective of the present invention to improve the staging and power efficiency of flow-through
15 capacitors. Power efficiency is a measure of how well power is distributed in a multi-cell system, and is defined here as the averaged percent of power needed by a flow-through capacitor system divided by the system's peak power needs. Staging efficiency is a measure of how well a staged system is designed to limit the inter-stage mixing caused by inter-stage dead volume, and is defined here as the percent
20 purification achieved by a multi-cell or multi-stage system divided by the sum of the percent purifications of each individual cell or stage. In the past, each cell or stage of a flow-through capacitor system has been housed within a separate housing or cartridge holders, which were charged or discharged together, either in parallel or in series. *See, e.g.*, US 2004/0121204 A1. A dead volume mixes with the water which
25 is purified in each stage, and decreases the resolution of the band of purified water, due to band broadening, as it moves from one stage to another. The mixing effect

also leads to a need to operate with greater numbers of stages, and may reach a lower voltage limit, as voltage is lowered when used with concentrated water such as sea water. Therefore, a need exists for an improved flow-through capacitor which has less mixing of purified or concentrated water with each other or with the feed water, and for a method and system which allows the capacitor to operate more efficiently at lower, energy saving voltages.

In addition, capacitors exhibit a charging characteristic whereby upon initial application of a voltage, they require peak power. Charging banks or stages of capacitors all at once multiplies this peak power, thereby increasing the wattage rating and cost of power supplies needed to provide this power. Therefore, an additional need exists to more efficiently distribute power to banks of flow-through capacitor cells which may be fluid or electrically staged in a combination of parallel or in series.

Summary Of The Invention

Sequentially powered and controlled flow-through capacitor systems of the present invention control individual flow-through capacitor cells, or groups of cells, in a timed sequence, with individual cells out of phase with each other. The system of the present invention may be configured with one cell per cartridge holder.

Preferably, the flow-through capacitor system is configured to have one or more integrated stages, by which is meant that two or more purification stages occupy a common housing, i.e., are within the same container or cartridge holder. When one flow-through capacitor cell represents a discreet purification stage, integral staging is achieved by housing two or more flow-through capacitor cells within a single container or cartridge holder.

The integrated stage design embodiment of the present invention eliminates the need, cost, and complication of connecting separate cartridge holders per stage by

containing multiple stages within the same cartridge holder. This integrated stage design reduces the band broadening that would otherwise be caused by mixing of the band of purified water with dead volume as it moves from stage to stage. Staging efficiencies of 50% or more are possible by using sequential charge cycles coupled with integrated stage design. Another advantage achieved by organizing a flow-through capacitor system so that some or all stages are physically integrated is to diminish the amount of dead volume that otherwise exists between the capacitor layers and the inside the walls of the cartridge holder or capacitor container.

The integrated stage design of the present invention incrementally sharpens purified and concentrated bands of feed solution as it flows from stage to stage. In individually staged capacitors of the prior art, a dead volume exists between each multilayer capacitor cell and the internal walls of the housing of the cartridge holder. In the integrated stage embodiment, each stage shares common capacitor material layers. Only the current collectors, or, where electrodes are conductive enough not to need a current collector, the electrodes, are independently actuated and electrically separated from each other. Therefore, multiple stages can share the same cartridge holder, thereby eliminating the need for separate current collectors. Eliminating excess dead volume through integrated staging allows operation of the capacitor at lower voltage while, at the same time, obtaining a deep purification peak. The result of this is that the capacitor may be operated at lower, more energy efficient voltages.

One special use of integrated staging is for low energy desalination of sea water. The present invention achieves that end by removing a little bit of salt at a time at low energy, and then amplifying this signal by virtue of synchronous charging of multiple capacitor stages that share the same capacitive material, spacer, and optional charge barrier layers in order to sharpen bands of purified and concentrated

water. This band sharpening method uses staging to refine or sharpen concentration bands, analogous to other staged methods such as chromatography, distillation, and absorption.

An additional advantage of the sequential charging system of the present invention is to provide power in steps between multiple cells in order to optimize peak power usage to allow use of lower wattage, less expensive power supplies, so as to avoid the requirement for peak power at the initial application of voltage and distribute power to banks, or stages, of flow-through capacitor cells which may be fluid or electrically staged in a combination of parallel or in series. By sequentially spreading out the application of peak power to individual cells in a multi-cell system, power efficiencies of up to 50% to 100% are possible. In other words, power usage may approach the averaged power needed over the sum of the individual cell cycles.

The flow-through capacitor of the present invention can make use of the same layers used in prior flow-through capacitors systems, such as, for example, US 6,413,409 and US 6,709,560 ("*Charge barrier flow-through Capacitor*"). Preferably, in a flow-through capacitor system of the present invention, in place of integral current collectors backing one or more electrode layers, multiple current collectors are arranged sequentially along a fluid flow path. In the integrated stage embodiment, these are arrayed within the same cartridge holder. These current collectors are made to be charged or discharged according to various sequences and times. The sequential charging of the multiple current collectors may either be done in series or in parallel, and in addition, within the context of either a series or a parallel flow cell.

Load leveling may be achieved by such sequential control of flow-through capacitors cells according to the present invention whereby capacitor cells are charged or discharged in a timed sequence. In doing so, the present invention avoids the

multiplication of peak power needs, thereby minimizing the size and cost of power supplies required to power a multiple flow-through capacitor system. The cells may be progressively powered or charged in parallel, or in series. If powered or charged in series, the voltage is stepped up as each cell is switched in an additive sequence onto the others in series. Parallel cells may be powered or charged by switching onto a common bus. Individual cells may have individual or common power supplies. Flow-through capacitor cells can be integrated within a single cartridge holder, or may be discrete cells in a combination of series or parallel electrical or fluid flow. Upstream cells within an integrated stage cartridge holder, or individual stages with one cell per cartridge holder, or groups of cells, may be charged first, then additional downstream stages or cells are charged with a time delay. Cells connected together, either singly or in groups, in parallel or series in an electrical or fluid flow sense, may be sequentially actuated or controlled according to the present invention. This time delay may be selected so that the peak capacitive charging peaks do not overlap, in order to obtain a lower average peak charging current.

It is desirable for the present invention to cut the peak wattage of power supplies needed by 30% to 50% or more. In order to level the watt, amperage, or power load of the flow-through capacitor system, charge cycles of individual cells or groups of cells, either in series or parallel, are preferably actuated sequentially, or between 1 and 359 degrees out of phase, such as by charging or discharging, or reversing the cell polarities in increments that vary between one and one hundred seconds. For example, cells can be charged or discharged in increments of between five and thirty seconds. Sequential operation of the charge cycles may also follow other patterns than the direction of flow. For example, where it is important to quickly reduce the output conductivity, it may be preferable to charge the downstream

cells first. In lieu of time, a voltage or an amperage sensor may relay data from individual cells to a logic chip or circuit in order to control the sequence of actuation of a series of flow-through capacitor cells or groups of cells.

The circuits used to distribute power to flow-through capacitor system preferably provide DC power in a sequential fashion in order to minimize the capacitive charging power surge. Circuits designed for stepwise charging of multiple batteries, multiplex charging or discharge of banks of batteries may be used to distribute power to the flow-through capacitor cells according to the present invention; examples of such circuit design include, without limitation, US 6140799, US 6326768, US 6140799, US6750631, US 5506456, US 5461264, US 5483643, US 5514480, and US 5710504 (each hereby incorporated by reference). Where batteries or battery banks are replaced by flow-through capacitor cells or capacitor banks, and with the addition of a necessary switches, relays, or FET circuits that sequentially switch in or switch out flow-through capacitor cells using a timer , voltage sensor, or amperage sensor logic of the present invention. Power sequencer circuits designed to distribute power across multiple loads, such as those known to those skilled in the art to be used to charge banks of batteries, capacitors, lights, motors, or other multiple loads, and preferably which are designed to avoid power surges when charging multiple loads, can be adapted to provide DC power and used in the flow-through capacitor system of the present invention, where the loads are multiple flow-through capacitors. Examples of a power sequencer circuit include, but are not limited to, US 6766222 and US 6239510 (each hereby incorporated by reference), circuits used in solar power distribution such as US 6685334 (hereby incorporated by reference) where the solar power source is replaced by a DC power source, power distribution circuits where DC power is provided or substituted for AC

- outputs and used to provide sequential power control according to the present invention. One example, without limitation, of a timer circuit that may be used for sequential control of flow-through capacitor cells according to the present invention is described in US 6011329 (hereby incorporated by reference). Power Field Effect
- 5 Transistors (FETS) or thyristors may be also used as mechanical contacts or relays in various timer circuits that may be employed, for one example, an H Bridge FET circuits such as described by Blanchard, Eugene
- (<http://www.armory.com/~rsteview/Public/Motors/H-Bridges/Blanchard/h-bridge.htm>; last visited August 6, 2004).
- 10 Power may be distributed to multiple stages of the present invention by using a power distribution or power management system circuits designed to control peak loads, or a sequential power distribution circuit. Useful examples of circuits that may be used, where the electric loads are multiple flow-through capacitor cells, include without limitation US 5119014, US 4093943, US 4180744, US RE29560,
- 15 US 6385057, US 5070440, US 5969435, and US 4894764 (each hereby incorporated by reference). In an additional embodiment, power sharing schemes where batteries, fuel cells, or generators are used to receive or give power to or from either the flow-through capacitor system of the invention or a prior art flow-through capacitor system may also be used. An example of such a power sharing system is described in, but
- 20 not limited by, US 5969435 (hereby incorporated by reference). The present invention may be combined with various power sharing circuits that may also be used to level the load, distribute power, or conserve energy during the charging of multiple capacitor cells or stages. Systems described for charging multiple batteries may be used, with capacitors replaced for some or all of the batteries. Examples are described

in but not limited to US 6444159, US 5757163, US 5955868, and US 6157867 (each hereby incorporated by reference).

A sequential power circuit similar to ones used to generate current pulses, including but not limited to US 4001598, US 5952735, and US 5585758 (each hereby
5 incorporated by reference) can also be used to sequentially charge and discharge flow-through capacitor loads to a power source in order to offset by between 1 and 100 seconds the peak amp and power requirements of individual flow-through capacitor cells in a multiple cell system. Failed or short circuited cells may be bypassed by using a current or voltage sensing or voltage drop circuit such as without limitation
10 US 6087035, US 5362576, and US5650240 (each hereby incorporated by reference) to close valves into or out of individual cells. In addition, another way to cut peak power needs is to use charged capacitors to power discharged capacitors, using an optional DC to DC converter between cells or series groups of cells to save additional energy if desired.

15

Brief Description Of The Drawings

Fig. 1 is a schematic illustration of an integrated stage flow-through capacitor and system of the present invention.

Fig. 2 is a detail view of a flow-through capacitor cell assembly.

Fig. 3 is an illustration of an integrated stage flow-through capacitor cell.

20

Fig. 4 is a schematic illustration of a spiral wound integrated stage flow

Fig. 5 is a representation of a nested current collector flow-through capacitor.

Fig. 6 is a representation of a series or series array flow-through capacitor.

Fig. 7 is an illustration of concentration stream manifold 22 and purification stream manifold 23 combining together the concentration streams 20 and purification
25 streams 21 produced by multiple electrode or electrode assembly layers 8.

Fig. 8 is a graphical illustration of sequential charging current of an eight cell flow-through capacitor system.

Detailed Description

Fig. 1 is a schematic of an integrated stage flow-through capacitor cell and system of the present invention, showing a controller or logic means 1, a power supply 2, e.g., a capacitor power supply, a switch power supply 3, ground 4, switches, relays, or FETS, e.g., switches 5, a cartridge or cell holder 6 as a casing for one or more capacitor cells, inlet 7, electrode or electrode assembly 8, outlet 9, flow path 10, individual current collector 11, individual current collector lead 12, circuit 13, e.g., an integrated circuit, programmable logic chip, digital input/out, or printed circuit; cell assembly 14, and sensor 15. A computer or controller 1 and a additional digital input/output 13 controls and actuates switches, relays, or FETS 5 in either a pre-programmed or feed-back controlled sequence using conductivity, pH, or other composition data, or flow, amperage, or voltage data supplied to controller 1 by sensor 15. Switch 5 can be multiple switching, and can also be an integrated circuit or chip with multiple outputs, can be triggered to ground 4 and thereby allow flow of current to current collector leads 12 into individual current collectors 11. Cell assembly 14 is made of electrode or electrode assembly layers 8 with flow spacer or spacers 16 (shown in Fig. 2), and individual current collectors 11. Multiple switching 5 can be controlled by a programmable chip, computer, controller, logic, timer, or in response to amp, voltage, or conductivity sensor data input, to sequentially charge or power the individual collector leads 12.

Fig. 2 represents a detailed view of a flow-through capacitor cell assembly 14 of the present invention showing optional electrical insulating spacers 15, insulating electrodes or electrode assemblies 8 one from the other. Electrode assemblies 8 are

backed by individual current collectors 11 which are individually connected to individually actuated electrical leads 12.

Fig. 3 represents an integrated stage flow-through capacitor cell of the present invention with individual current collectors 11, current collector leads 12, against electronically conducting electrode or electrode assembly 8. The electrode or electrode assembly 8 is spaced apart by flow space or flow spacer 16 with optional flow or series electrical isolation gaskets 14. Flow path 10 is shown cutting across the multiple current collectors 11 connected to individual electrical leads 12. The multiple current collectors shown in Fig. 3 may be thin enough to be wires, for example, less than two millimeters in diameter.

Fig. 4 represents a spiral or concentric flow-through capacitor of the present invention with electrodes or electrode assembly 8, flow path 10 intercepting multiple current collectors 11 connected to individual electrical leads 12.

Fig. 5 represents a nested integrated stage flow-through capacitor single electrode assembly layer 8 with associated individual current collectors 11 and current collector leads 12, flow path 10 and flow inlet our outlet.

Fig. 6 represents a flow-through capacitor of the present invention with a matrix series connection such that individual cells may be connected in series both horizontally and vertically. Fig. 6 illustrates cartridge holder or capacitor casing 6, inlet or outlet 7, outlet or inlet 9, current collectors 11, individual current collector leads 12, and series separator 18, and high resistive series cell separator flow path 10. Only individual current collectors 11 and current collector leads 12 are shown, with the addition of inter-cell series separators 18. An optional high resistive flow path 19 is included for use when current collectors 11 are connected in series across the stack. Either a parallel or a series cell, not shown, would be placed between the end current

collectors 11. Where series cells are used, and where each of these cells is in turn connected in series, the resulting capacitor cell would form a series matrix, with resulting voltage upon charge of the matrix the multiple of the series voltage of the individual cells times the number of series cells further connected together in series.

- 5 Cartridge holder or capacitor casing 6 contains the matrix connected flow-through capacitor formed by these components plus additional electrodes or electrode assembly layers 8 and flow spacers 16 shown in Fig. 2

Fig. 7 represents a flow-through capacitor of the present invention with the flow parallel to the current collector 11, which may be used to provide continuous
10 concentration streams 20 and purified solution flow channel 21 to provide a purification stream. Concentration stream 22 is a flow channel for concentrated solution. Purification stream 23 is a flow channel for purified solution. Concentration stream 22 and purification stream 23 are connected by manifolds so as to combine together the concentration streams 20 and purification streams 21
15 produced by multiple electrode or electrode assembly layers 8.

In Fig. 8, curves I1 through I8 represent eight separate charging currents of eight flow-through capacitor cells sequentially charged at constant voltage in an eight cell integrally staged flow-through capacitor system. Optionally, constant current schemes can also be used. This charging scheme can be applied to either integrated or
20 individual flow-through capacitor cells. Notice how each current trace, I 1 through I 8, has a typical capacitive charging shape, with peak current in the time equals less than one seconds, then leveling off rapidly after that over a period of 1 to 60 seconds or more. If, for example, the multiple cells have been charged together in parallel or in series, there would only have been one charging curve with a maximized peak
25 wattage. This is undesirable because it requires a larger, more expensive power

supply. By offsetting the peak amperage and power curves as in Fig. 8, the additive power is reduced. Optimally, the additive power can be averaged over multiple cells in this way, to comprise the average power usage over a charge cycle averaged over a number of cells. The charge cycles can be synchronized to correspond with the arrival of a traveling purification segment or peak as it moves serially from cell to cell, in order to trigger progressive removal of total dissolved solids from that purification peak. Flow can also be parallel through a number of cells with asynchronous charge cycles. A charge cycle may be a combination of constant voltage, constant current, reverse polarity, and optional shunt cycles, with each such portion of a charge cycle lasting between zero and 300 seconds or more, for example 60 seconds, or 5000 seconds. Charge cycles between individual flow-through capacitor cells may be asynchronous or out of phase between one quarter and 300 seconds or more, for example, 100 seconds or 10,000 seconds. Charge cycles may be triggered by a timer, a conductivity reading, a voltage, a pH, or other data. Valves to individual cells or groups of cells that dispose of waste, delivered purified fluid, or which recycle in flow loops may be triggered synchronously or asynchronously together with the above charge cycles. For example, it may be desirable to trigger individual valves from individual cells in a multi-cell system at the same time the purification or waste part of a charge cycle is triggered. The purified product or concentrated waste segments of water from individual cells or cell groups may subsequently be combined together, such as through a manifold, in order to maximize the level of purification or concentration, for example, to than 40% purified and better than 40% recovery or more, for example 90%.

In one embodiment, the integrated stage flow-through capacitor of the present invention utilizes multiple current collectors 11 individually connected to current

collector leads 12 with common flow path layers 14, and electrode or electrode assembly layers 8 that may be optionally separated by inter electrode insulators 19. The current collectors are multiple in the sense that a plurality of current collectors are transected by a common flow path 10, share common electrode or electrode assemblies 8, or are placed within the same cartridge holder or capacitor casing 6. A stage is represented by a pair of current collectors typically perpendicular to, but optionally parallel to, the flow path 10. Flow path 10 therefore typically intersects oppositely charge current collector pairs. As the fluid in flow path 10 flows across these current collector pairs, the current collectors, through individual current collector leads 12, are activated in a sequence. This sequence can either be programmed or may be triggered by a sensor 17. Each time a pair of current collectors is activated with a voltage, additional materials are either removed from or added to a band of water which flows from cell to cell, where cell may be defined as a oppositely charged pair of current collectors charged together in time as part of a charge sequence among many pairs of current collectors. The multiple current collectors 11 of the present invention within each cartridge holder may bracket a stack of electrode assemblies 8 that are electrically insulated from each other in true series fashion, such as in US 6628505 (hereby incorporated by reference), or the current collectors can be bundled together in parallel, to form anode and cathode, with geometries as known to those skilled in the art, including but not limited to the geometries of US 5,192,432, *"Flow Through Capacitor"*; US 5,196,115, *"Controlled Charge Chromatography System"*; US 5,200,068, *"Controlled Charge Chromatography System"*; US 5,360,540, *"Chromatography System"*; US 5,415,768, *"Flow-Through Capacitor"*; US 5,538,611, *"Planar, Flow-Through, Electric, Double Layer Capacitor And A Method Of Treating Liquids With The Capacitor"*; US 5,547,581, *"Method Of*

separating Ionic Fluids With A Flow Through Capacitor"; US 5,620,597, *"Non-Fouling Flow-Through Capacitor"*; US 5,748,437, *"Fluid Separation System With Flow-Through Capacitor"*; US 5,779,891, *"Non-Fouling Flow-Through Capacitor System"*; US 6,127,474, *"Strengthened Conductive Polymer Stabilized Electrode Composition And Method of Preparing"*; US 6,325,907, *"Energy And Weight Efficient Flow-Through Capacitor, System And Method"*; US 6,413,409, *"Flow-Through Capacitor And Method Of Treating Liquids With It* (each of which are hereby incorporated by reference). Those skilled in the art will also be guided by WO93/13844, *"Chromatography System With flow-Through Capacitor And Method"*; WO94/26669, *"A Planar, Flow-Through, Electric, Double Layer Capacitor And A Method Of Treating Liquids With The Capacitor"*; WO95/21674, *"Flow-Through Capacitor And Chromatographic System And Method"*; WO97/13568, *"Non-fouling, Flow-fouling, Flow-Through Capacitor system And Method Of separation"*; WO00/14304, *"Flow-Through Capacitor And Method Of Treating Liquids With It"*; WO 01/09907 A1, *"Flow-Through Capacitor And Method"*; WO 01/13389 A1, *"Flow-through Capacitor system And Method"*; WO 01/66217 A1, *"Low Pore Volume electrodes With Flow-Through Capacitor And energy Storage Use And Method"*; WO 01/95410 A1, *"Fluid and electrical connected flow-Through Electrochemical Cells, System Cells, System And Method"*; and WO 02/29836 A1, *"Fringe-Field Capacitor Electrode For Electrochemical Device"*. In addition to the stacked layer geometries shown here, individual electrodes shown in the electrode array WO 03/009920 A1 may be sequentially charged according to the present invention in order to form flow through capacitor stages according to the present invention.

The electrode assembly 8 can include a combination flow-through capacitor electrodes and optional current collector, ion perm selective membranes, or charge barrier material. (US 6709560, hereby incorporated by reference). For example, the electrode can be comprised of high capacitance particles, including carbon or

5 ceramics, held together with a binder material including a hydrogel or functional charge barrier material, fibrillated polypropylene or PTFE, latex, or cross linked or sintered polymer or hydrocarbon materials. For example, if a charge barrier material is used as a binder, it may be a fluorine containing ionomer, an elastomeric or thermoformable hydrogel containing either or both of strong acid or strong base

10 functionality. Materials of use as charge barriers are known to those skilled in the art. (See, e.g., Toshikatsu Sata, Ion Exchange Membranes, The Royal Society of Chemistry, publ., 2004).

An important aspect of the invention is the ability to vary the voltage, current, or power, either perpendicular or parallel to the flow path within a single cartridge

15 holder, or among a group of single cartridge holder cells. In the integrated stage embodiment, this is accomplished by incorporating multiple current collectors within a single cartridge holder, where the current collectors can have individual electrode, charge barrier, and flow spacer layers, or can share one or more of these layers in order to simplify manufacture. A fluid, solution, or solute to be purified of

20 concentrated is introduced into each cell. As this fluid flows through each cell, the multiple current collectors are independently synchronously actuated with a purification or a concentration peak that forms as the flow moves through each cell. This is analogous to the peaks formed in chromatography systems. For example, a small amount of total dissolved solids can be purified from water each time the flow

25 stream passes a particular current collector, or pair, or set of current collectors. This

produces a slightly purified aliquot of water. As this aliquot moves along its flow path, additional current collectors are actuated. Where this flow path cuts across multiple current collectors, the flow stream is separated into purification and concentration peaks that can be separated, e.g., by a valve. Where the flow is parallel
5 to the multiple current collectors, the fluid will be separated into side by side purification and concentration streams.

Where electrode layers are shared between multiple current collectors, it is important that the current collectors are electrically isolated. To do this, the distance between current collectors has to be wide enough so that the current collectors have a
10 fair degree of electrical isolation between them. Generally, wider than one sixty-fourth of an inch, and optimally, under three inches, such as between one eighth and one quarter inch, will suffice to isolate the cells. Cells are sufficiently isolated when the width between current collectors backing an adjacent electrode material of a given conductivity is such that the overall conductivity of the combined current collector –
15 electrode combination is 1 ohm cm or greater. Resistance between individual current collectors is preferably 0.1 ohm or more.

Prior flow-through capacitor systems reach a practical limit of efficiency due to the fact that less total dissolved solids and other contaminants are removed from water per charge cycle as voltages are lowered. The flow rate utilization per gram of
20 carbon needs to be lowered in order to provide a given percent purification at a lowered voltage and energy usage level. This slowing of the flow rate was necessary in prior systems, because sufficient levels of purification must be maintained in order to overcome the mixing effects of the cartridge holder dead volume. The capacitor of the present invention minimizes this cartridge holder dead volume by eliminating
25 inter-stage cartridge holders. For example, with integrated staging, the dead volume

due to the flow spacer may be larger than the dead volume due to the volume that exists between the capacitor cell and the inside of the cartridge holder. The capacitor cell is defined as the electrode, flow spacer, and a current collector and charge barrier layers. Therefore, focused bands of purified water may be obtained at low voltages and therefore low energy usage levels. An advantage of the present invention is that energy may be saved by charging an integrated stage cell many times at lower voltages. Percent utilization of the cell may be increased by virtue of operating the cell so that more than one concentration band is present at a given time within a given material layer or cartridge holder. To obtain purified water at a desired purification level, a valve coupled with a conductivity sensor selects out water desired purification and concentration levels. Percent recovery may also be pre-selected by presetting conductivity control based upon a mass balance between purified, feed, and/or waste concentrations.

An additional advantage of the present invention is that it allows operation without a valve, achieving continuous purification. In this case, flow may be parallel to the current collectors, and fluid concentration may be modulated within the plane of the flow. Fig. 7 depicts how water may be purified in purification stream 21 between one set of current collectors and concentrated in concentration stream 20 between adjacent sets of current collectors, with purification streams 21 and concentration streams 20 being coplanar in the direction of flow. These coplanar streams are brought together by, e.g., manifolds, to form a continuously purified stream 23 and concentrated stream 22. Optionally, ions can be manipulated by operation of the current collectors in order to form a central flow path of one concentration and side flow paths of another. In either case, adjacent concentration bands are formed which may be directed to separate collections paths or separately

collected from separate outlets in the cell casing provided for this purpose. A valve is not except when it is desirable to switch concentration and purification streams by polarity reversal or otherwise electronically manipulating the charge cycle sequence.

Individual current collectors may be pre-manufactured onto electrode layers
5 by lamination or by continuously coating a banded pattern of current collector material onto an electrode material. The current collector material may be a conductive material less than 1 ohm cm in resistance, including a graphite material, or, may be a metal foil, in particular, metal foil protected by a conductive vinyl or a form of carbon-polymer composite layer using carbon black, nanotubes, graphite
10 powders, etc. mixed in with a thermoplastic, olefin, fluorocarbon, or a other polymer, used with a metal backing to form a current collector where the metal is protected from water by the thin polymer layer, with the polymer layer typically under 0.03 cm thick. Conversely, a capacitance containing electrode material may be discontinuously formed in a banded pattern upon a suitably conductive current
15 collector layer. A carbon containing material may be used. Microparticulate titanium oxide powder is also advantageous.

Electrode materials may include carbon black, activated carbons, sintered carbons, aerogels, glassy carbons, carbon fibers, nanotubes, graphite, and other forms of carbon in particular those with surface areas over 400 BET, nanotube gels,
20 conductive polymers, ceramics, anatase titanium oxide, or another material that has a capacitance above 1 Farad per square meter when applied in a layer 0.1 cm or less thick. A binder material may be used which holds the electrode capacitive particles together, including hydrogels, latex, thermoplastics, and fluoropolymers. Charge barrier materials may be an ion exchange polymer, hydrogel, cross linked polymer, or
25 membrane, preferably with a charge density of over 0.1 milli-equivalents per gram.

The charge barrier material can also function as a binder or adhesive, which is used cause capacitance containing electrode particles together to form an electrode sheet, or to adhere them to a current collector.

To manufacture the present invention, current collector, electrode, and a
5 charge barrier layers may be laminated or layered together in a stacked configuration, then cut to length and inserted into a cartridge holder. As many layers as can be cut effectively at one time are layered and pre cut together. The blocks of materials so formed can in turn be layered on top of one another and inserted into a cartridge holder designed to fit them. Current collector tabs may overlap out either end, and be
10 bundled together in parallel or connected in series. If graphite foil is used as a current collector, the end tabs may be infiltrated with an oily material or a polymer so that they do not wick water. A metal compression contact may be formed with a nut, bolt, and-or washer arrangement to the bundled graphite tabs. This contact may be protected from water by a compression nut containing a gasket which screws down
15 over the top in order to cover underlying metal contacts. Inert metals such as titanium, tantalum, including palladium or platinum coated or infused valve metals, may be used to form metal to graphite contacts. It is preferable that contact resistance be less than 1 ohms. Metal contact to graphite compression over 10 psi, and metal to graphite contract areas over 1 cm² may be used to achieve this.

20 In Fig. 8 the current declines with each successive charge. This is because a volume of feed water was being successively purified as it passed through each of the eight sequentially charged cells. As the water becomes more purified, it increases the resistance as it passes through subsequent cells, thereby causing them to draw less current and power. The fact that all the cells are not charged at once allows the
25 purification peak to be deepened, allowing greater peak purification, for example,

50% purification or more. Using integrated flow-through capacitors to cut dead volume we have been able to achieve 70% purification of sea water in an eight cell system at only 0.3 Volts. Based upon energy measurements in single cells, this low voltage is likely to be in the 15 watt hour per gallon range. Significant purification in the 20% range has been measured with as low as 0.1 volts, which represents very little energy. The percent purification can be increased by adding a sufficient number of stages.

Cells within a sequentially controlled train of flow through capacitor individual cell stages need not all be the same size. For example, downstream cells, which experience a partly purified stream of water compared to upstream cells, may be sized smaller in order to save cost, or in order to design shorter charge cycles that match the charge cycles of upstream cells. On the other hand, a downstream cell may also be sized larger where it is important to increase the percentage of purification or concentration in the last stage compared to the previous stages.

CLAIMS

What is claimed is:

- 5 1. A flow-through capacitor system comprising a plurality of flow-through capacitor cells, each of said plurality of cells in electrical communication with a charge cycle sequence controller.
2. The flow-through capacitor system of claim 1, further comprising a plurality of current collectors and a flow spacer are shared among said plurality of
- 10 current collectors.
3. The flow-through capacitor system of claim 1, which is operated such that multiple concentration bands exist simultaneously within a given material layer.
4. The flow-through capacitor system of claim 1, further comprising a conductivity controlled valve between at least two of said plurality of current
- 15 collectors.
5. The flow-through capacitor system of claim 1, further comprising a flow stream parallel to at least two of said plurality of current collectors, with continuous purification and concentration streams directed to separate collection paths.
6. The flow-through capacitor system of claim 4, wherein fluid is manipulated
- 20 to form adjacent purification and concentration streams that may be separately collected without need for a valve.
7. The flow-through capacitor system of claim 1, wherein valves are individually triggered with charge cycles in order to produce a purified product stream.
- 25 8. The flow-through capacitor system of claim 1, wherein said flow-through capacitor system has a staging efficiency of 50% or more.

9. The flow-through capacitor system of claim 2, wherein said flow-through capacitor system has a power efficiency of 50% or more.

10. The flow-through capacitor system of claim 1, wherein the charge cycles of individual cells are synchronized to correspond with the arrival of a segment of
5 purified water traveling in serially through multiple cells.

11. The flow-through capacitor system of claim 1, wherein voltage is incremented in a step wise fashion as cells are sequentially powered by adding them in series.

12. The flow-through capacitor system of claim 1, wherein cells are powered
10 by sequentially switching them together in parallel.

13. The flow-through capacitor system of claim 1 whereby the voltage varies along the flow path.

1/8

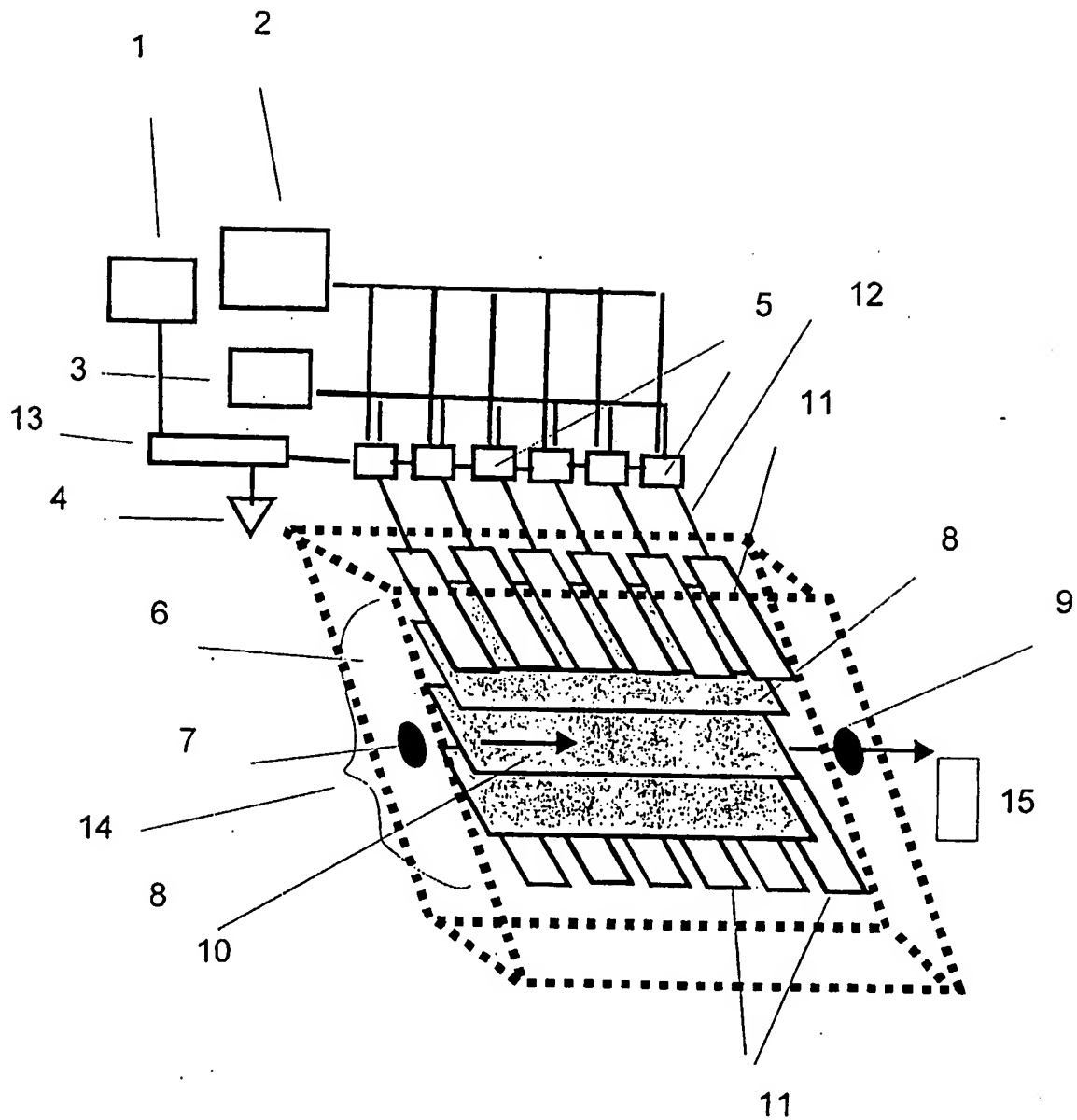


Figure 1

2/8

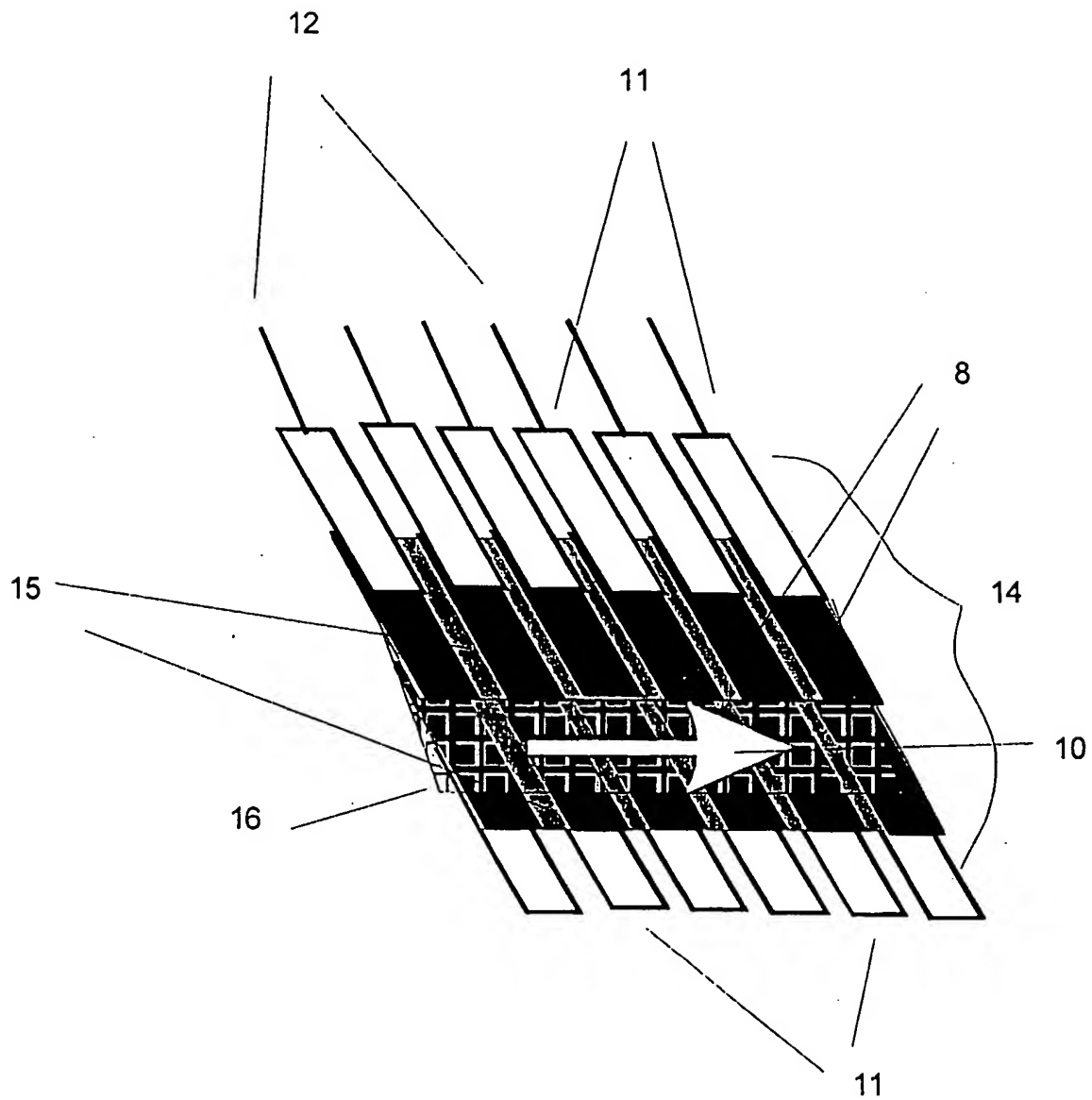
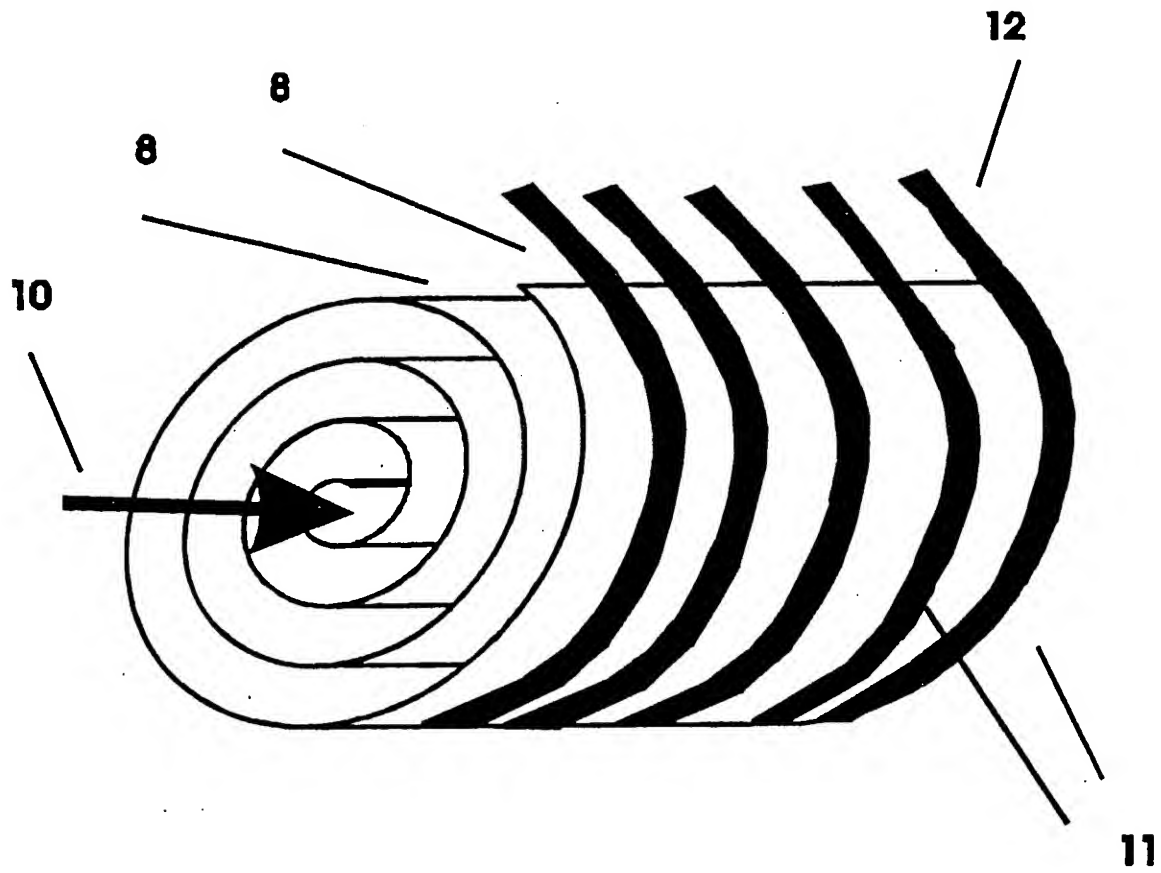


Figure 2

4/8

**Figure 4**

5/8

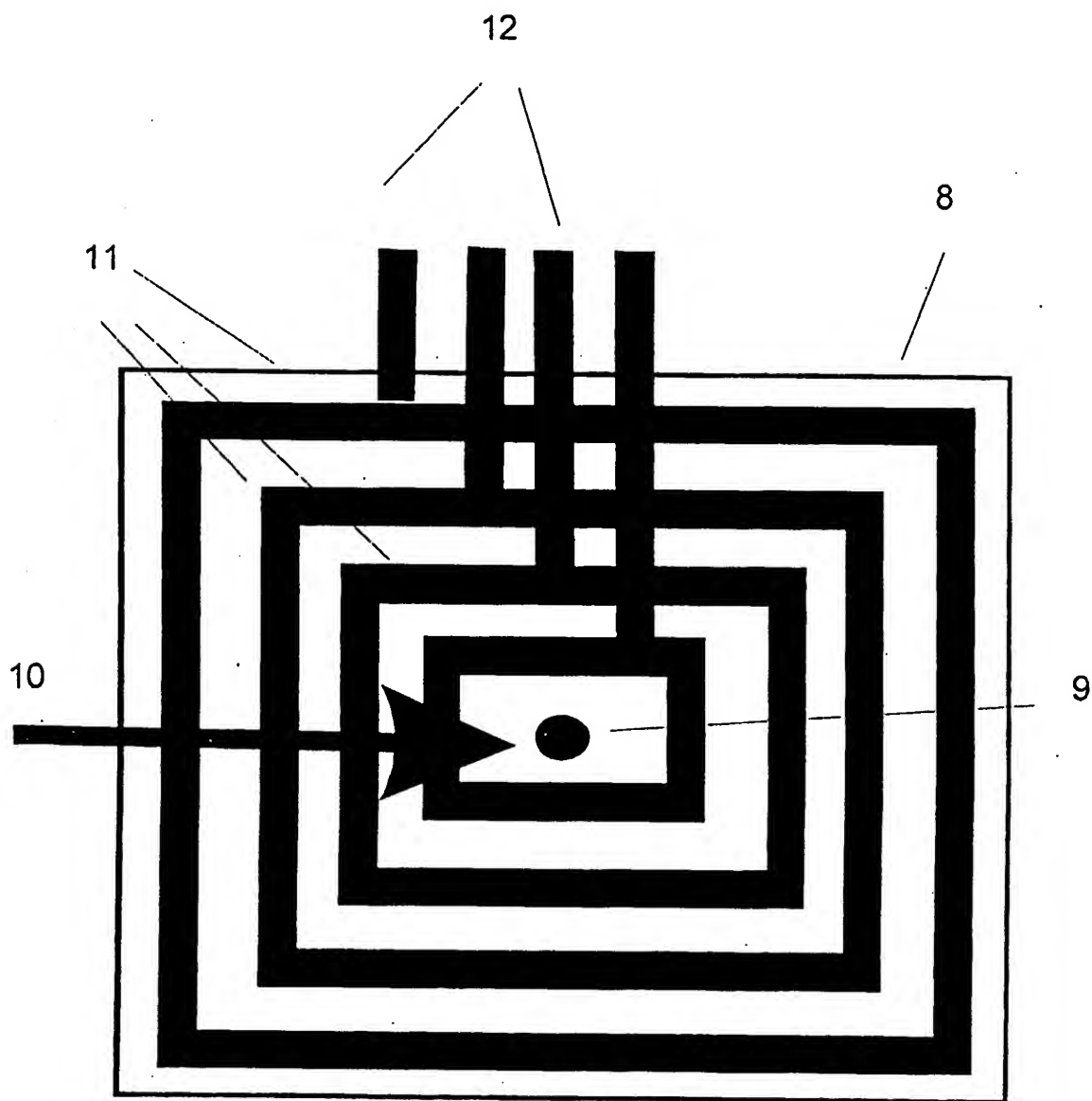


Figure 5

6/8

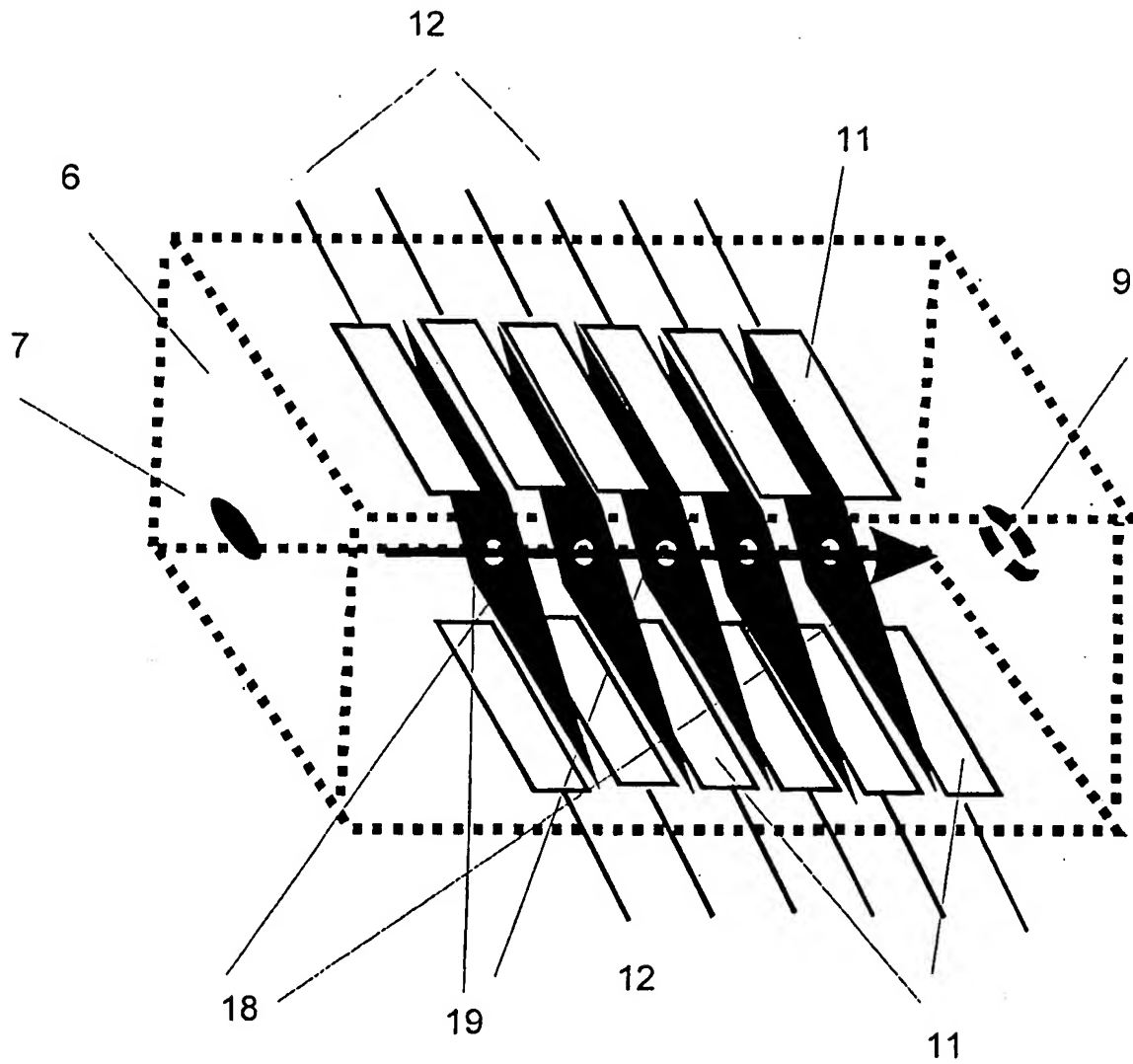


Figure 6

7/8

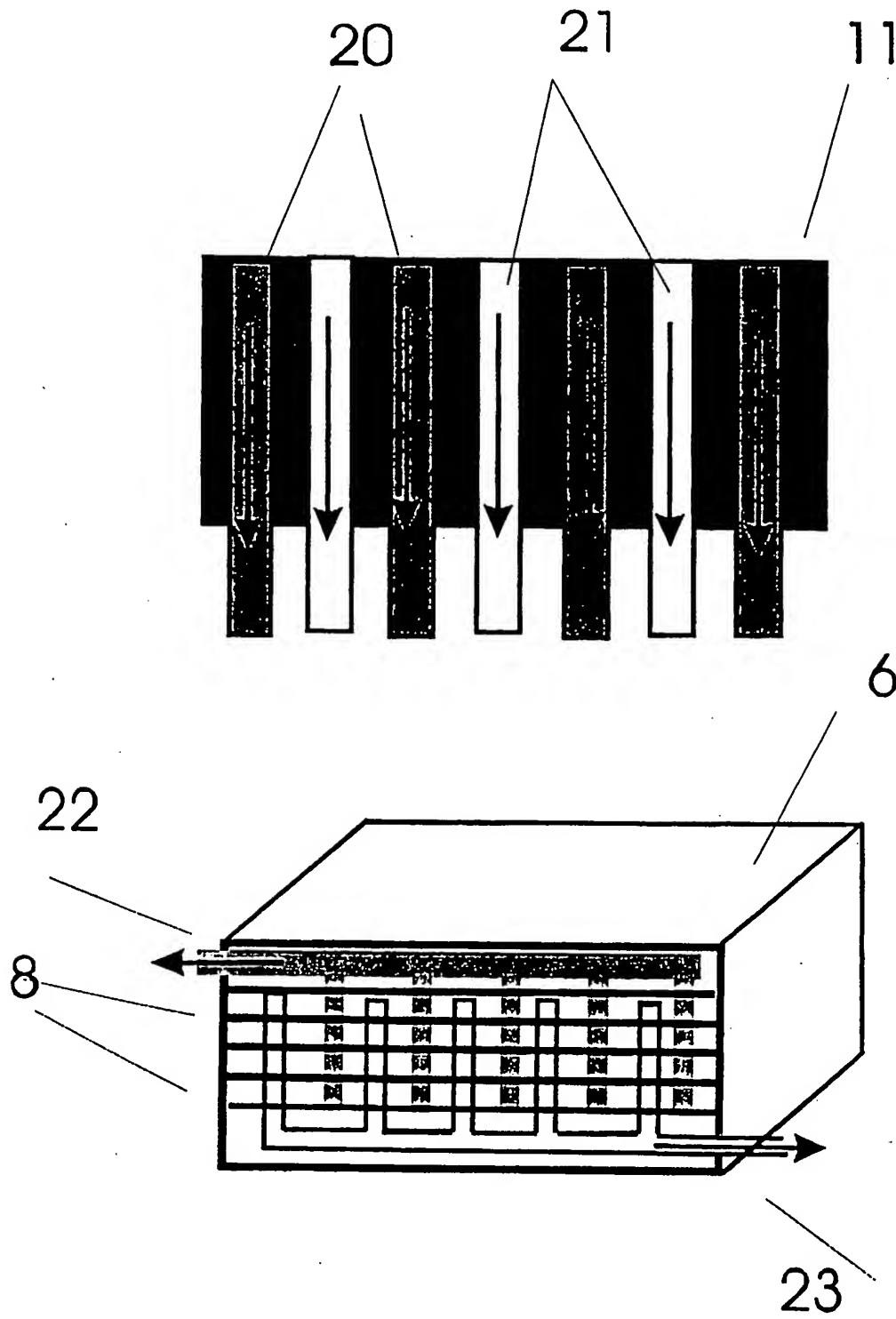
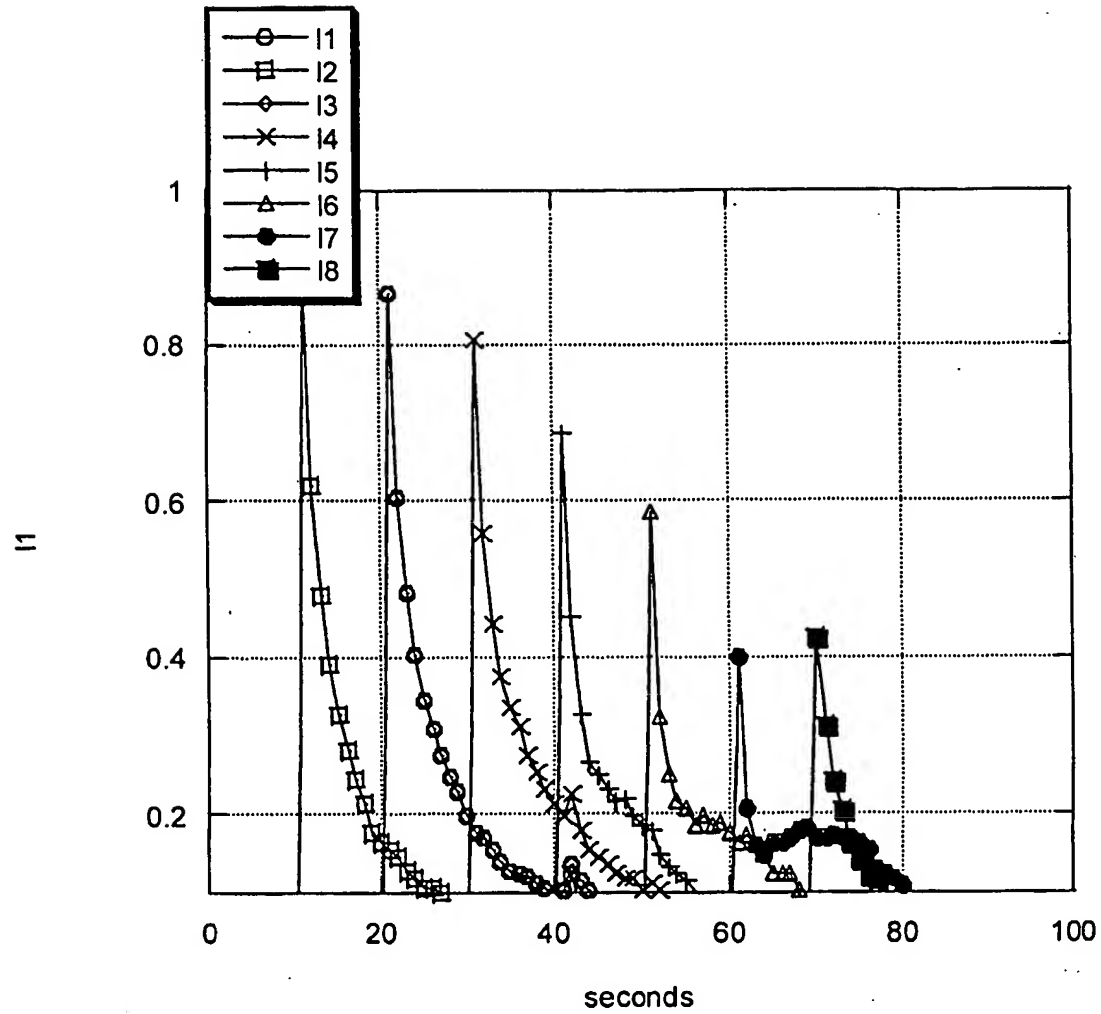


Figure 7

8/8

Figure 8